Constructal design of gas-cooled electric power generators, self-pumping and atmospheric circulation

A. Bejan, S. Lorente, J. Lee, Y. Kim

Duke University, Department of Mechanical Engineering and Materials Science, Durham, NC 27708-0300, USA
Université de Toulouse, INSA, 135 Avenue de Rangueil, 31077 Toulouse, France
Doosan Heavy Industries & Construction Co., Ltd., 22 Doosan Volvo-ro, Seongsan-gu, Changwon, Gyeongnam, South Korea

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Abstract
Rotating electric machines generate heat volumetrically, and are cooled by forced convection aided by the self-pumping effect. In this paper we focus on the fundamental relationship between the internal flow architecture of the gas cooled winding and its thermal performance, which is represented by the nearly uniform distribution of peak temperature throughout the winding volume. We show that the cooling passages can be sized such that the volumetric cooling is most effective. From this finding follows the number of passages and their distribution through the heat generating volume. The principle is developed analytically, and it is then validated based on numerical simulations of the cooling architecture. The paper also reports the thermodynamics basis of the self-pumping effect, and its natural occurrence as free convection in general, which includes atmospheric circulation.

1. Introduction

In this paper we take a look from above at the improvements that can be made in the performance of cooling architecture of synchronous electric power generators for steam power plants. The focus is on fundamentals. The approach is based on constructal design [1,2] which is the philosophy that improvements in global performance are achievable through continuous changes in the geometry of the flow system, to facilitate flow. For this purpose, the flow architecture must be free to morph, and the better and better flow architectures must be pursued relentlessly.

What designers view as “optimal” is the time direction in which the architectural changes are happening. The direction is natural, and is exhibited by the evolutionary designs of mammal systems (the evolution of technology) and, even more visibly, by the flow architectures of nature [2]. The natural evolutionary character of technology was illustrated recently by the evolution of aircraft [3].

Here we focus on the evolutionary design of gas-cooled synchronous generators powered by steam turbines in modern power plants [4–6]. The synchronous generator is a solid structure that generates heat volumetrically, and is cooled by a gas that flows through multi-scale channels embedded in the structure. The design of the structure (sizes, materials, shapes, connections) is the result of trade-offs between several key objectives: mechanical strength, stiffness, electromechanical power conversion, heat transfer (cooling) and fluid flow [7,8].

Traditionally these objectives were pursued separately, and the features that satisfied one objective served as constraints in the pursuit of features that satisfy the other objectives. More recently, computational design is making possible the search for features that satisfy several objectives simultaneously. Electric machines of all kinds are evolving toward compactness, which means higher power density. In this direction, the generation of heating per-unit volume increases, and so do the peak temperatures that threaten the mechanical integrity and electrical performance of the machine. Effective volumetric cooling is of paramount importance in the future of electric machines.

In this paper we address the fundamentals of the volumetric cooling of the machine structure. The approach is based on constructal design, which is the view that the heat and fluid flow structure morphs freely as we search for a higher heat transfer density, lower peak temperatures, and a more uniform distribution of the allowable temperature level throughout the machine volume. Key are the continuous changes in the geometry of the solid, in the direction of greater compactness.
2. Configuration

The cooling gas enters the volume of the generator as a single stream. The channels distribute this stream throughout the volume such that the coolant bathes the smallest features of the heat generating structure. Finally, the warmed up coolant is reconstituted as a single stream and is led to an external system to be cooled before being reused (Fig. 1).

Heat is generated non-uniformly in three dimensions. The stator structure generates and conducts heat longitudinally along the bars and radially along the laminations. The stator structure is hierarchical: laminations are stacked into packages that are swept by coolant, and packages are grouped into sections that are permeated by coolant that flows in a particular radial direction, toward the axis, or away from the axis. Heat is also convected radially along the cooling channels. The key feature to be discovered is the channel spacing, or the number of packages in one section (Fig. 2).

In current designs, the rotor winding has the highest heat generation density. Its heat and fluid flow structure (Figs. 3 and 4) is similar to the stator structure. Heat is generated and conducted longitudinally in the electrical conductors of the magnetic field winding. Heat is intercepted by the coolant and convected radially through radial spacings. The flow of coolant through the rotor is always outward, toward the relative motion gap between rotor and stator.

In summary, the flow of heat is in steady-state, from the cylindrical volume of the machine to the stream of coolant that flows through the volume. The coolant flows through multiple channels: it is distributed non uniformly and hierarchically though few large and many small channels. A fan drives the flow of coolant. In the rotor, the flow is augmented (aided) by the self-pumping effect that emerges when the coolant is heated by the solid structure. Self-pumping is another name for natural convection (or chimney flow) through radial channels. The pressure difference generated by this effect is given in Section 4.

The cross sectional shapes of the rotor and stator volumes with heat generation and radial flow are annular. In each annulus, the radial thickness is not much larger than the inner radius. Consequently, the annular space can be modeled as a two-dimensional space, as shown in Fig. 5. The radial dimension of this space (H) is the radial length traveled by the coolant. The axial dimension of this space (L) is the distance between two consecutive cooling channels. The channel spacing (S) and the solid thickness (D) may vary.

In the rotor (r) and the stator (s) the conduction through the spaces filled with solid (the windings) is anisotropic. In the rotor, the axial thermal conductivity (kax) is greater than the radial conductivity (kar). In the laminations of the stator, the opposite is true: the radial conductivity (kar) is greater than the axial conductivity (kax).

The anisotropy of the stator is complicated further by the thermal conductivity of the stator bars (kbs), which is greater than kax and kcar. The fluid flow through the stator is also complicated by the fact that the channel flows may be oriented in counterflow, unlike the parallel flows through the rotor winding.

3. Parallel flow

Consider one of the heat generating volumes (in the rotor, or the stator, Fig. 6), and treat it as a two-dimensional volume of longitudinal length Lr (the rotor length), transversal flow length H, and third dimension πD, where D is the diameter of the relative motion gap. The total heat generation rate removed from this volume is q. The total mass flow rate of fluid that bathes this volume is m.

There are n radial slits of flow length H and spacing S, where n = Lr/L, and L is the axial dimension of each heat generating section kbar, cf. Fig. 6. The coolant is an ideal gas. It enters the slit at the temperature T0, and exits at the temperature Tout, which is to be determined. The maximum allowable temperature (Tmax) occurs at hot spots located in the exit plane, midway between two consecutive exits. The objective is to configure the flow such that (Tmax – T0) and the fan (pump) power are small when q and m are specified. In the limit of small S and large n, the flow through the volume resembles Poiseuille flow through parallel-plates channels (Fig. 7, left). In this limit, Tout approaches Tmax and the entire plane with the outlets is isothermal, at Tmax. The coolant (m) enters the volume at T0, and exits at Tmax therefore q = mcP(Tmax – T0). The performance is indicated by the ratio

\[
\frac{T_{\text{max}} - T_0}{q} = \frac{1}{mcP}
\]

(1)
This comes at a cost in pressure drop, because $\Delta P$ in Poiseuille flow increases fast as $S$ decreases Ref. [1, p. 113],

$$\Delta P \sim \frac{m}{n} \frac{H}{S^2}$$  \hspace{1cm} (2)

In the opposite limit, the spacings $S$ are large enough so that the fluid temperature is $T_0$ throughout the channel volume (Fig. 7, middle). In addition, assume that the flow along each channel (with small $\Delta P$, because $S$ is large) is fast enough so that the surfaces of the channel are essentially at $T_0$. This means that the removal of the heat generation rate is limited by solid conduction in the axial direction (perpendicular to the channel), where $k_x$ stands for either $k_{rx}$ or $k_{sx}$,

$$q \sim 2n k_x \pi D H \frac{T_{max} - T_0}{L/2}$$  \hspace{1cm} (3)

which yields

$$\frac{T_{max} - T_0}{q} \sim \frac{L^2}{4\pi k_x H D L_r}$$  \hspace{1cm} (4)

The third design to consider is in-between. It is the design with constructal spacings (Ref. [1, Ch. 3]), in which $S \sim 2\delta$, and $\delta$ is the thickness of the laminar boundary layer that lines every surface of flow length $H$ (Fig. 7, right). If the flow is laminar, then, in an order of magnitude sense,

$$\delta \sim 3HRe_{H}^{1/2}$$  \hspace{1cm} (5)

where $Re_H = VH/\nu$. The factor 3 appearing in Eq. (5) is an approximation of the factors appearing in the Blasius solution (factor 4.92) and the displacement-thickness solution (factor 1.73) [9]. The mean fluid velocity along the channel is

$$V = \frac{m}{n} \frac{H}{\rho S \pi D}$$  \hspace{1cm} (6)

The spacing is therefore

$$\frac{S}{H} \sim 10^2 \frac{D L_r}{\pi L}$$  \hspace{1cm} (7)

The solid thickness $L$ is determined as follows. The total heat transfer rate is expressed in two ways,

$$q = mc_p(T_{out} - T_0)$$  \hspace{1cm} (8)

$$q = 2nH\pi D k_x \frac{T_{max} - T_{out}}{L/2}$$  \hspace{1cm} (9)

where we assumed that the channel surface is at $T_{out}$. Combining Eqs. (8) and (9) we obtain

$$\frac{T_{out} - T_0}{T_{max} - T_{out}} \sim \frac{4\pi k_x H D L_r}{mc_p L^2}$$  \hspace{1cm} (10)
Next, the continuity of heat flux at the fluid–solid interface requires

\[ k \frac{T_{\text{out}} - T_0}{S/2} \sim k_0 \frac{T_{\text{max}} - T_{\text{out}}}{L/2} \]  

which yields

\[ \frac{T_{\text{out}} - T_0}{T_{\text{max}} - T_{\text{out}}} \sim \frac{k_0 S}{k L} \]  

Note that in Eq. (11) we wrote \( k \) for the fluid thermal conductivity, and because the fluid has a Prandtl number close to 1, the thermal boundary layer thickness is the same as the velocity boundary layer thickness, \( \delta \sim S/2 \). Combining Eqs. (10) and (12) we arrive at

\[ SL \sim 4\pi \frac{kHDLcP}{c_p m} \]  

which agrees with Eq. (7) because the Prandtl number \( \nu/\alpha(= \mu c_p/k) \) is a constant of order 1. Note that \( S \) increases when \( L \) decreases, and vice versa.
The figure of merit \((T_{\text{max}} - T_0)/q\) is obtained by eliminating \(T_{\text{out}}\) between Eqs. (8) and (9),

\[
\frac{T_{\text{max}} - T_0}{q} \sim \frac{1}{\dot{m}C_p} + \frac{L^2}{4\pi HDkL_r}
\]

(14)

This shows that the lowest level of peak temperatures corresponds to the small-\(S\) limit represented by Eqs. (1) and (2). Small packages (\(L\)) approach the limit of Eqs. (1) and (2).

4. Self pumping

The pressure drop for this design continues to be given by Eq. (2), which is the same as writing

\[
\Delta P \sim \frac{\dot{m}vHL}{L_rS^4}
\]

(15)

Because \(SL\) varies as \(1/\dot{m}\), cf. Eq. (13), we conclude that \(L \sim 1/(\dot{m}S)\) and consequently the pressure drop varies as \(S^{-5}\). The pumping power that is required to overcome \(\Delta P\) has the order of magnitude

\[
W = \frac{\dot{m}\Delta P}{\rho} \sim \frac{\dot{m}^2vHL}{\rho L_rS^5}
\]

(16)

In the rotor, the self-pumping effect reduces the \(\Delta P\) by a fraction that can be estimated as follows. As shown in Fig. 8, the cold coolant enters along the rotor axis at the temperature \(T_0\). The coolant is then accelerated to the rotor radius \(R\) (the relative motion gap), where its pressure and temperature increase to \(P_R\) and \(T_R\).

We assume that the rotor radius is considerably smaller than the rotor length, such that most of the heating experienced by the \(\dot{m}\) stream occurs at high pressure, at the rotor radius, in the windings. According to the same model, the flow of \(\dot{m}\) in the radial direction is approximated as reversible and adiabatic:

![Fig. 5. Parallel flow versus counter flow through a two dimensional conducting body with internal heat generation.](image)

![Fig. 6. Parallel flow model of a gas-cooled stator structure.](image)

Fig. 5. Parallel flow versus counter flow through a two dimensional conducting body with internal heat generation.

Fig. 6. Parallel flow model of a gas-cooled stator structure.

![Fig. 7. The two extremes of the flow structure of Fig. 5: from small spacings, Eq. (1), to large spacings, Eq. (14).](image)

Fig. 7. The two extremes of the flow structure of Fig. 5: from small spacings, Eq. (1), to large spacings, Eq. (14).
When the heating effect is negligible ($\tilde{q} < 1$), the self-pumping effect indicated by Eq. (23) is negligible,

$$\frac{P_{\text{out}}}{P_0} \sim 1$$  (26)

We return in Section 6 to the self-pumping effect and its occurrence in nature.

5. Number of core packages

In this section, we report the results of numerical simulations of the heat transfer in the rotor, and the effect of the number of core packages. As a first step, we select the domain in which to model numerically the very complicated architecture of the generator. The problem is three-dimensional because of the presence of the longitudinal bars. Key is the search for symmetry planes that will allow to simplify as much as possible the numerical simulations. Longitudinally, we have a sequence of core packages (thickness $W_c$) and gas spacing (thickness $S$), as shown in Fig. 2. This sequence leads to the existence of the two first planes of symmetry that we will use in the modeling. The longitudinal dimension of the control volume is $(W_c + S)/2$.

The height of the domain is set by the height of the core packages, $H_c$. The focus must be on the stator part of the generator. Therefore we add to $H_c$ the distance between the outer radius of the rotor and the inner radius of the stator, $d_a$ (Fig. 3). $H_c$ and $d_a$ are fixed. We also add to the height of the computational domain a distance located at the outer radius of the stator.

We repeat the procedure in the transversal direction with the objective to discover the planes of symmetry where they exist. The stator bar is made of 42 elemental bars positioned radially and separated by a constant angle (Fig. 9). The outer radius of the bars is named $r$, while $W_b$ is the transversal thickness of each bar. The gas gap between two bars is called $L_e$, and is calculated as $2\pi r = 42(W_b + L_e)$. The combination of gas gap and bar leads to two new planes of symmetry, one in the bar, and the other one in the gas gap. The thickness of the control volume in the transversal direction is therefore $(W_b + L_e)/2$.

In summary, the control volume (Fig. 9) is modeled as a parallelepiped with the dimensions:

- Height: $d_a + H_c + d$
- Longitudinal thickness: $(W_c + S)/2$
- Transversal thickness: $(W_b + L_e)/2$, where $L_e$ is the spacing between bars.

As an example for the numerical simulations, we choose $d_a = 10$ cm, $H_c = 70$ cm, $d = 10$ cm, $W_b = 2.5$ cm, $L_e = 8$ cm. The total volume of material is fixed, together with the size of the generator. Furthermore, the core height is also fixed, because of mechanical and electrical constraints. The degree of freedom will be the longitudinal thickness, and its components $W_c$ and $S$. In other words, we study the allocation of the combination of material & fluid so that the maximum temperature reached by the material remains below $T_{\text{max}}$.

Fig. 10 shows the control volume, the stator tooth, the stator bar and the stator yoke. The final version of the control volume with the four domains to model can be seen in the fifth drawing of Fig. 10. The remaining volume (the difference between the control volume and the four solid parts) is occupied by the flowing fluid. The configuration is one of heat transfer and fluid flow, with conduction heat transfer in the solid. We model heat conduction inside the different types of solids and forced convection in the fluid. The fluid is hydrogen, and the flow is turbulent. We chose the $k$-$\varepsilon$ turbulence model, and solved the conservation of mass,
The boundary conditions are specified on four planes of symmetry in the transversal direction, one inlet in the longitudinal direction at the exit from the rotor, and one longitudinal outlet at the exit from the stator. The inlet temperature is moderate.

In addition, we attributed a volumetric heat density to each solid part: core tooth, core yoke and bar. The core yoke and tooth are made of SiO\(_2\). We applied a non-isotropic thermal conductivity by stating that the transversal thermal conductivity is five times larger than the conductivities in the other two directions. The bar is made of copper.

The coolant is hydrogen. Even though helium is inert and non-flammable, it cannot be obtained sufficiently in quantities, which makes its price high and makes it unsuitable as cooling medium. Hydrogen can be obtained rather inexpensively, and it has advantages over helium in having a small density and better thermal characteristics. These factors combine to make hydrogen an ideal coolant, but there is one major flaw that it is explosive when mixed with air and exposed to an ignition source. However, if the purity of the hydrogen gas can be maintained at a very high level, then, an explosion does not occur even if an ignition source is present. The hydrogen mass flow rate provided by the rotor rotation is fixed, and so is the inlet velocity. The inlet velocity is 2 m/s, corresponding to about 40 m/s near the bar.

Assume that the total rotor length is \( L \) (fixed), and the core length is \( L_{c1} \). If we have \( n_{c1} \) cores, then \( n_{c1} \times L_{c1} = L \). If one core is made of \( n_{1} \) channels, then \( L_{c1} = n_{1} \times (W_{c1} + S_{1}) \). The total mass flow rate is \( n_{c1} \times n_{1} \times m_{1} \) with \( m_{1} \) as a function of \( \dot{V}_{\text{inlet,1}} \times (W_{c1} + S_{1}) \).

If we have \( n_{c2} \) cores, then \( n_{c2} \times L_{c2} = L \). If one core is made of \( n_{2} \) channels, then \( L_{c2} = n_{2} \times (W_{c2} + S_{2}) \). The total mass flow rate is \( n_{c2} \times n_{2} \times m_{2} \), with \( m_{2} \) as a function of \( \dot{V}_{\text{inlet,2}} \times (W_{c2} + S_{2}) \). Because \( L = n_{c1} \times n_{1} \times (W_{c1} + S_{1}) = n_{c2} \times n_{2} \times (W_{c2} + S_{2}) \), we conclude that the model numerically. For each simulation we extracted from the results the maximum temperature. We found that the maximum temperature is always located in the vicinity of the bar, as one would expect.

Fig. 11 shows the maximum temperature as a function of the number of core packages. If the maximum admissible temperature is known, then the designer can select the number of core packages and the corresponding gap between them such that the solid reaches the maximum temperature value.
Fig. 12. The natural circulation of the atmosphere in the plane of the meridian is driven as a heat engine, which is equivalent to the self-pumping effect discussed in Fig. 8.

Fig. 13. The reverse of the circulation shown in Fig. 12 is impossible, because by itself the heat current Q does not flow from cold to hot.

Fig. 11 also shows that increasing the number of core packages has the effect of decreasing the maximum temperature. Interesting is that most of the decreases in $T_{\text{max}}$ occurs as $n_c$ increases to approximately 20, above which the decrease in $T_{\text{max}}$ is marginal as $n_c$ increases to 50. Because the simpler design is preferable, $n_c \approx 20$ is an important feature to seek for the design of stator cooling. This conclusion confirms the existence of an optimal spacing, cf. Fig. 7 and Eq. (14). The Reynolds number based on the swept length ($H_s \approx 30 \text{ cm}$) and mean fluid velocity (30 m/s) is of order $1.5 \times 10^5$. The boundary layer thickness is of order 0.25 cm, therefore the optimal spacing is of order 0.5 cm. This is in agreement with the spacing $S$ that corresponds to $n_c \approx 20$ in Fig. 11, because $S_r \approx 10 \text{ cm}$ is the total cooling spacing, therefore $S \approx S_r/n_c = 10 \text{ cm}/20 = 0.5 \text{ cm}$.

6. Conclusions, and atmospheric circulation

The main conclusion is that the path to increasing the cooling performance of the rotating electrical machine is by allowing the geometric features of the flow architecture to vary freely, on the way to decreasing the temperature peaks, wherever they may occur. This approach is in accord with the evolutionary direction sketched in Section 1.

For example, we showed that the allocation of the gas volume has a profound effect on decreasing the peak temperatures, cf. Fig. 11. Important is the conclusion that the act of increasing the number of core packages reaches diminishing returns. There is a critical number ($n_c \approx 20$) above which further increases in $n_c$ and flow architecture complexity do not yield significant decreases in the peak temperature.

On a more fundamental level, the thermodynamics basis of the self-pumping effect (Section 4) sheds light on all the phenomena of natural circulation that occur at all scales in nature. The earth-size equivalent of the flow of Fig. 8 is shown in Fig. 12, which represents the circulation of the atmosphere in the plane of the meridian. The atmospheric layer has the finite depth $h$, which is much smaller than the meridian length scale. Near the tropics, the air is warm (average density $\rho_w$) and the bottom-top hydrostatic pressure difference is of order $\Delta P_w \sim \rho_w g h$. Near the polar circle, the air is colder (average density $\rho_c$) and the bottom top hydrostatic pressure difference is of order $\Delta P_c \sim \rho_c g h$.

Note that $\Delta P_c > \Delta P_w$ because $\rho_c > \rho_w$. Furthermore, because the pressure at the upper surface of the atmosphere is uniform (zero), $\Delta P_w$ and $\Delta P_c$ represent the pressure exerted by the atmosphere on the ground. It follows that from the polar circle to the tropics, the pressure drop at ground level is of order $\Delta P = \Delta P_c - \Delta P_w \sim (\rho_c - \rho_w) g h$. This pressure difference drives the entire circulation, against friction. The pressure difference is due to the fact that at ground level (i.e., at high pressure) the cold air that descended from the upper levels is heated by the solar heat current $Q$, absorbed originally by the earth’s surface. As the circulation is completed at the upper levels, flowing from the tropical regions to the polar regions, the air current is cooled by radiation to the cold sky.

In sum, the circulation of air in Fig. 12 is the same as the circulation of the working fluid in a Rankine cycle or Brayton cycle, in this sequence: heating at high pressure is followed by cooling at low pressure. This is analogous to the sequence of processes identified in Fig. 8, although in that figure the cooling of in at low pressure (in the stationary frame of the laboratory) is not shown. The self-pumping effect that occurs in gas-cooled rotating windings is the same physics as all the natural circulation phenomena recognized broadly as natural convection, free convection, and buoyancy driven flow. The g of Fig. 12 plays the same role as the $\omega R$ of Fig. 8.

Equally important is the observation that the circulation explained in Figs. 8 and 12 cannot proceed in the opposite sense. Cooling at high pressure (at ground level) cannot happen after (or before) heating at low pressure (at upper levels). The reverse flow sketched in Fig. 13 is impossible because, by itself, the heat current $Q$ does not flow from the cold sky to the warm surface of the earth. Note also that the circulation imagined in Fig. 13 is the same as the circuit executed by the working fluid in a vapor compression or Brayton refrigeration cycle. In order to run (to force a heat current from cold to hot), a refrigerator requires an external power input. There is no external power that could drive the heat flow shown in Fig. 13.

In conclusion, self-pumping and heat-engine circulation (Figs. 8 and 11) occur naturally, as part of physics. The “refrigerator” circulation (Fig. 13) is impossible.

Conflict of interest

None declared.

References


